



# 29<sup>th</sup> Annual Spring Symposium—SPE

## Flare Gas Monetization: Plan, Measure, Act

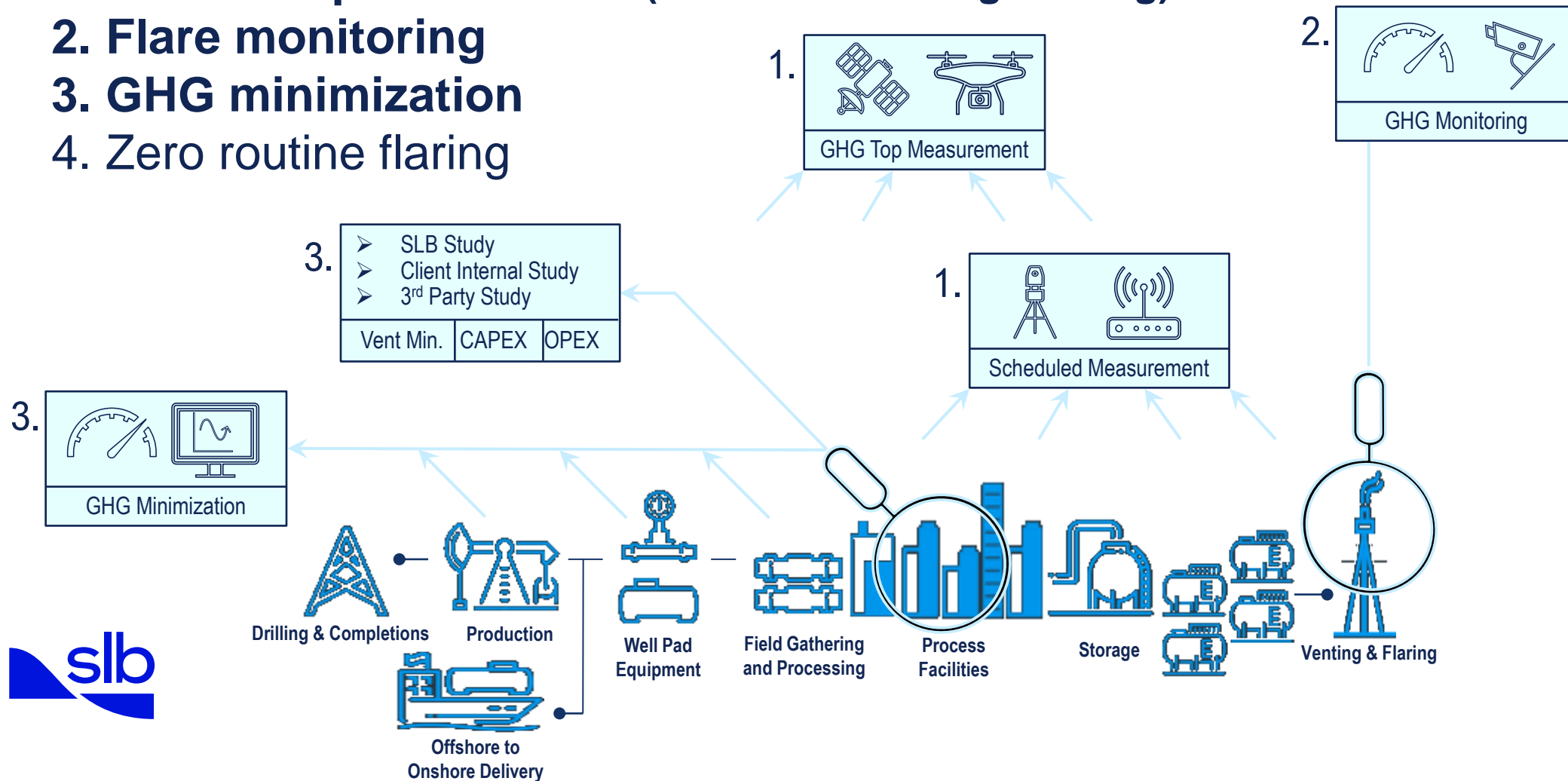
Glen Hay, SLB End-to-end Emission Solutions (SEES)

April 2024

# Emissions reduction—Planning towards zero emissions

## Steps

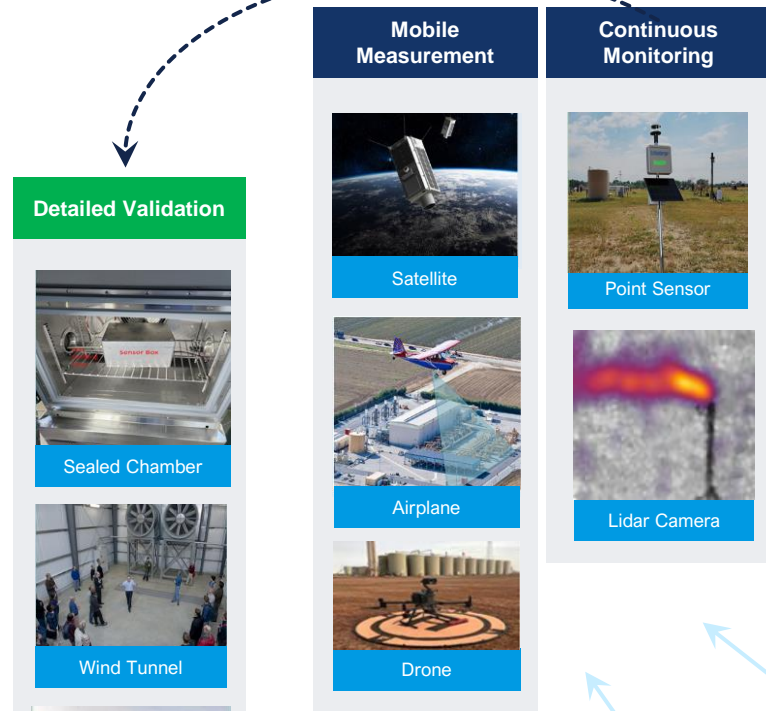
1. Methane quantification (measurement/engineering)
2. Flare monitoring
3. GHG minimization
4. Zero routine flaring



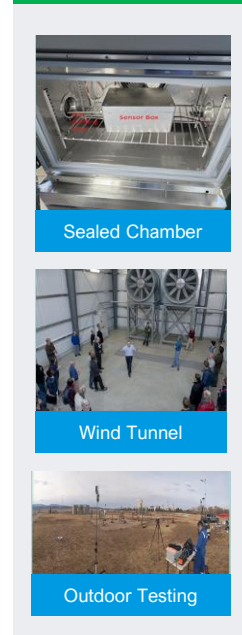
# Measuring and tracking GHG emissions

How do we handle measuring and estimating different emissions?

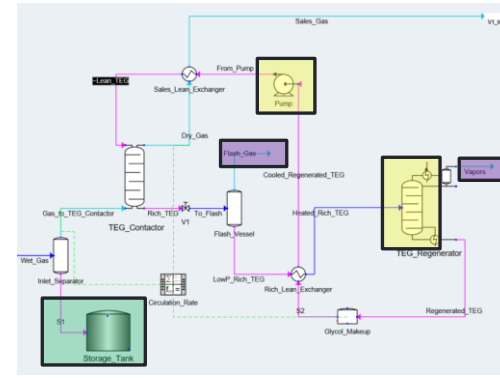
Measurements



Detailed Validation




## TEG Dehydration Plant Simulated Example

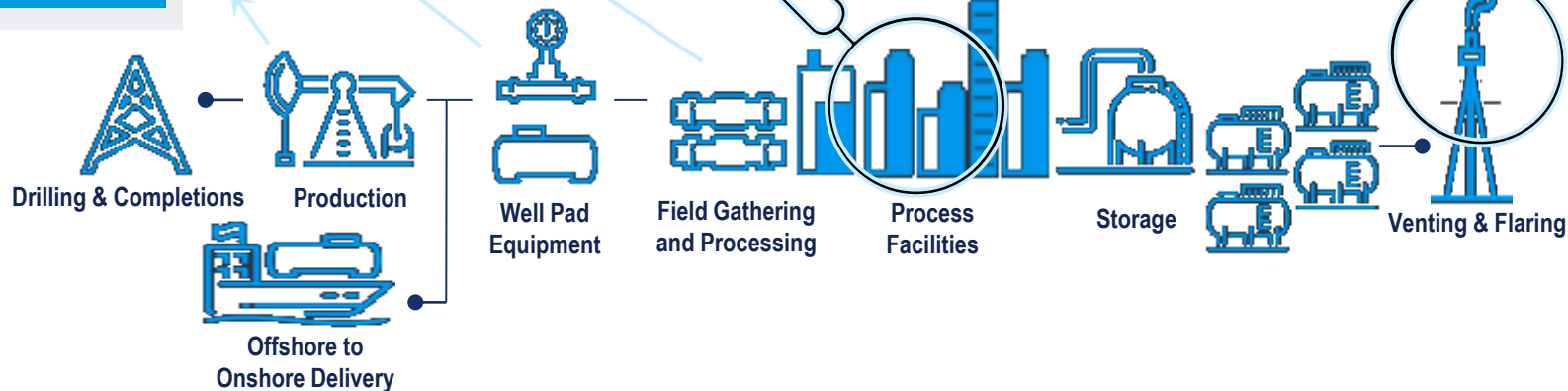


Engineering

### Inventory:

-  Storage Emissions
-  Venting & Flaring Emissions
-  Utility Related Emissions

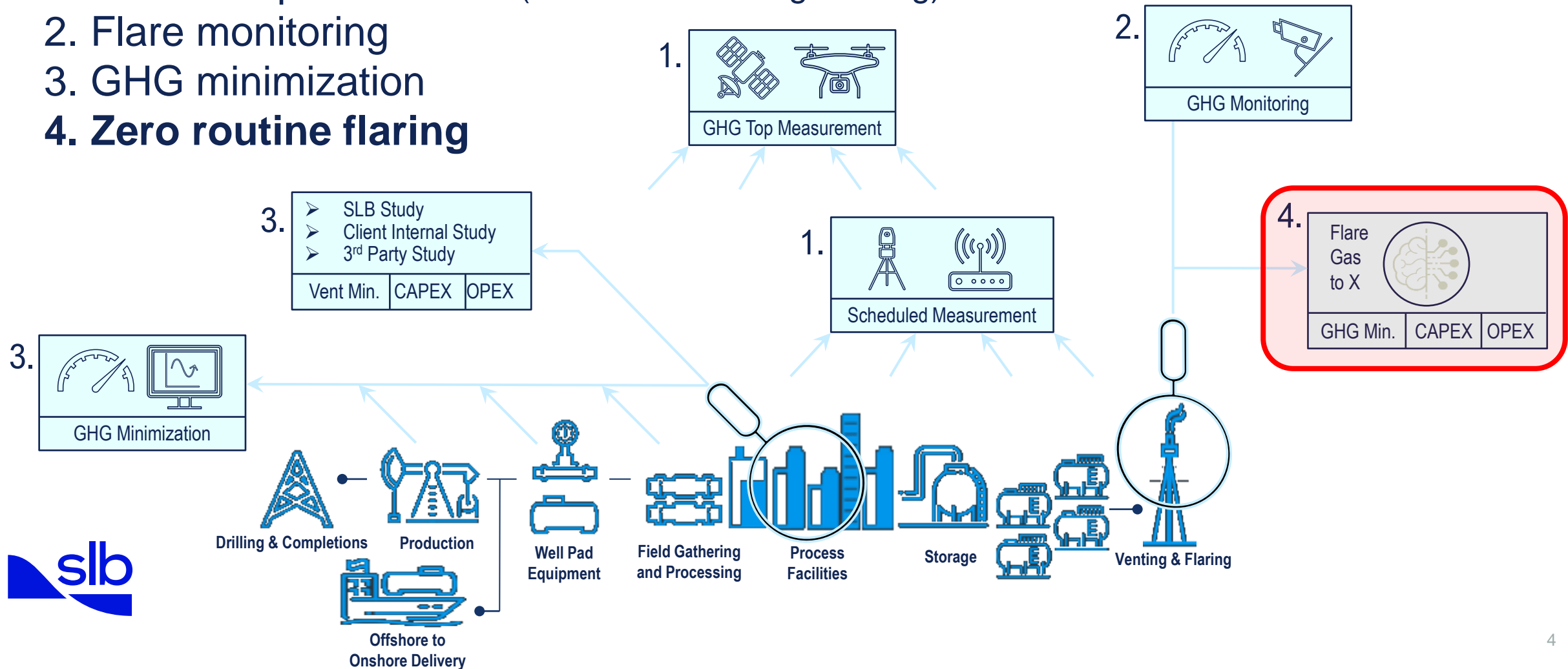
COMBINED



# Emissions reduction—Planning towards zero emissions

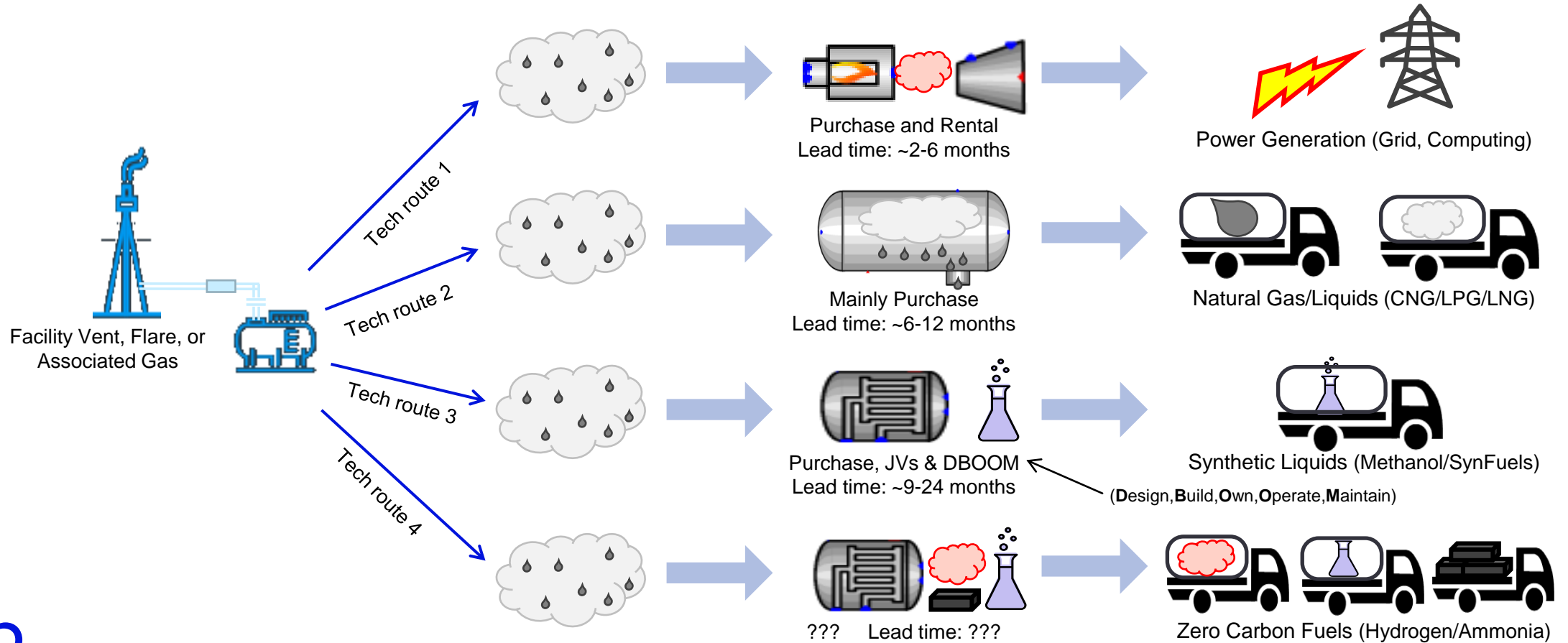
## Steps

1. Methane quantification (measurement/engineering)
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- 4. Zero routine flaring**



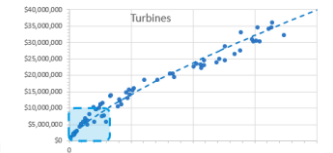
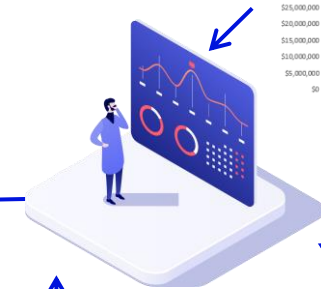
# Flare gas monetization—Major technology options

Flare elimination solutions for power, natural gas/liquids, synthetic liquids, and zero carbon fuels

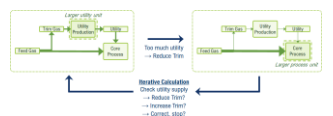
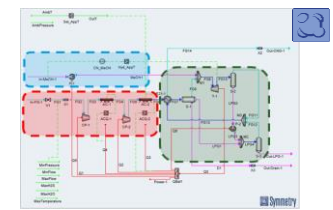


# Flare gas monetization— Overall “best” solution considerations

Economically optimized zero routine flaring

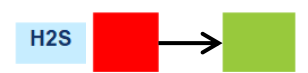
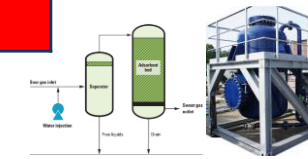


Micro Solution  
CAPEX/OPEX



Rigorously Balanced Utilities  
↳ Water, Power, etc.

What solution(s) will succeed most in the short and long term?

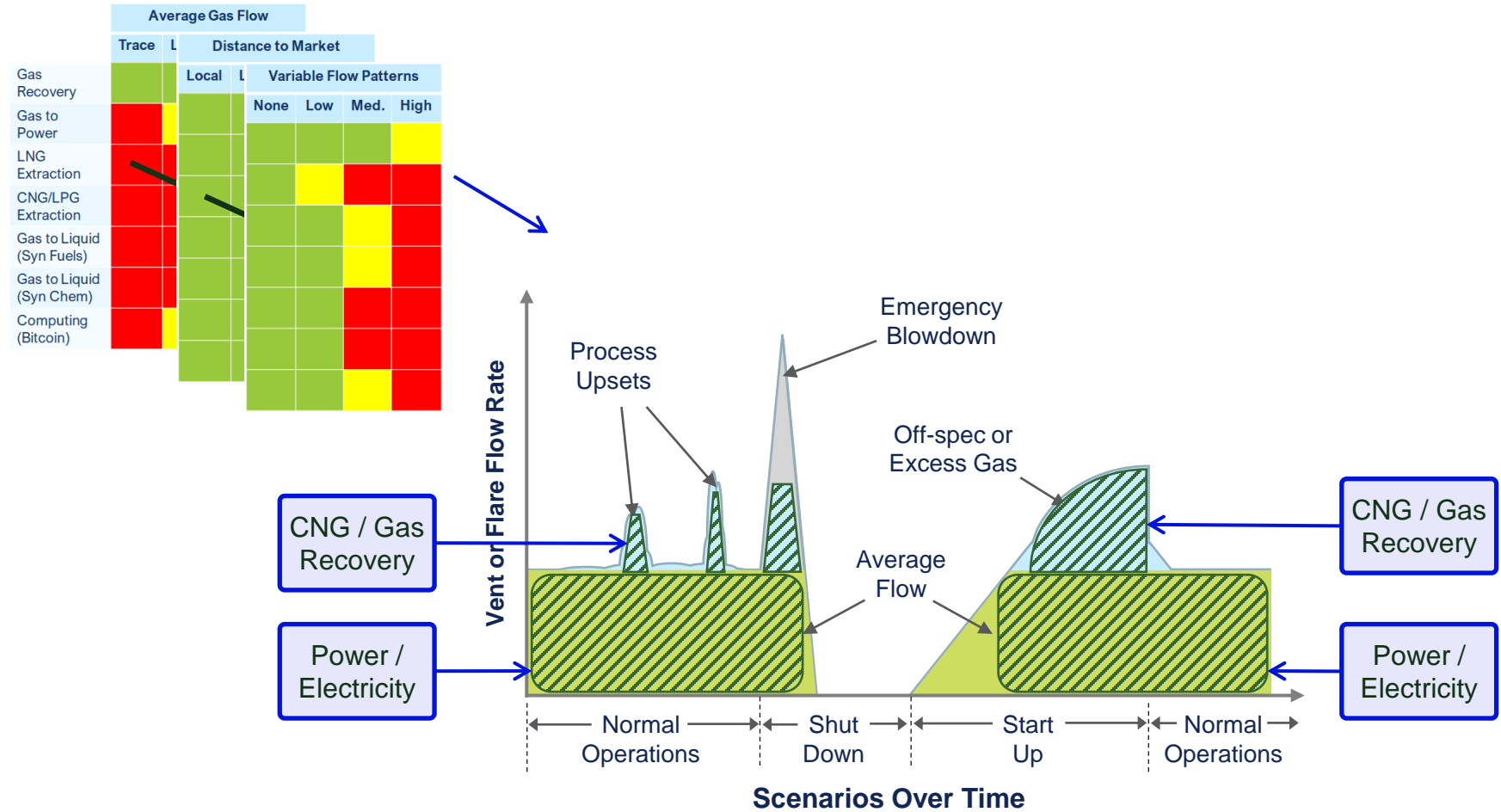


Integrated Overall Solutions  
↳ Pre-treatment and Post-treatment



# Flare gas monetization— Overall “best” solution(s) considerations

Economically optimized might be combined solutions



Reference: Flaring and venting guidance, Oil & Gas Authority (2021)

# Flare gas monetization— Power generation (grid, computing) and natural gas/liquids (CNG/LPG/LNG) overview

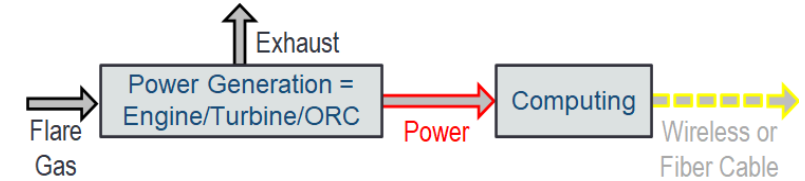
## Power generation to local utilization (rigs, injection, ESPs), grid, or computing power

Engine = Low feed  $H_2S$ , ~98%  
destruction efficiency  
Many units required  
for larger MW scale

Turbine = Lower OPEX, higher CAPEX,  
high feed pressure, more scale  
Aeroderivative Turbine even  
more CAPEX, less OPEX

Organic Rankine Cycle  
= Lower efficiency, flexible feed gas

Computing = Alternative market value generation



Very mature tech, but small grid power connection a hard sell

Solutions started with Bitcoin...  
now in AI, CFD, Bio-  
Computations, etc.  
(high bandwidth locations)

CNG/LPG Extraction (Chiller Loop or Expansion) = High feed pressure, water removal  
(or hydrate inhibition with methanol)

Solvent extraction more complex and high CAPEX and OPEX for smaller scale units <5 MMSCFD

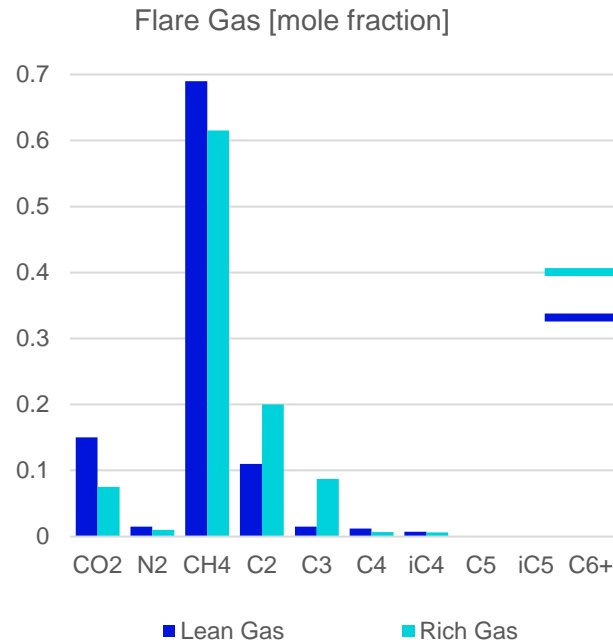
LNG Cryogenic (Chiller Loop or Expansion) = High feed pressure, water/ $CO_2$  flow assurance





# Flare gas monetization— Natural gas/liquids (CNG/LPG) logistics

Without conversion, feed gas composition dictates profits



\$ [redacted] / MMSCFD
\$ [redacted] / MMSCFD
\$ [redacted] / MMSCFD
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Depending on CAPEX and OPEX of the facility and markets the Initial Rate of Return (IRR) can shift from 25% to 50%

~4-year payback  
~2-year payback

FG = Flare Gas (sometimes more or less valued heavy components) (can contain H<sub>2</sub>O, CO<sub>2</sub>, N<sub>2</sub>, H<sub>2</sub>S, etc)

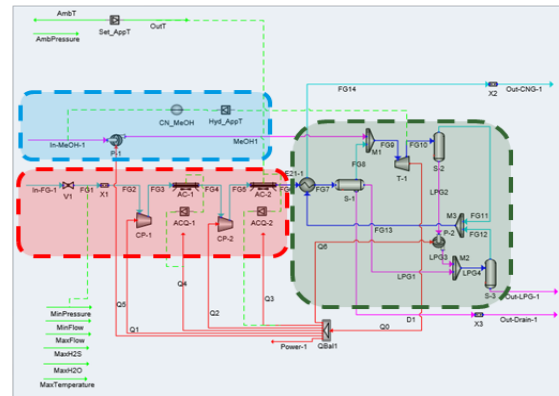
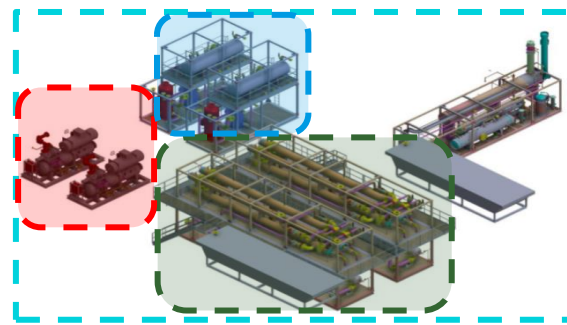
Std Liq Volume	[m3/h]
METHANE	8.456
ETHANE	2.231
PROPANE	2.110
n-BUTANE	0.986
ISOBUTANE	0.479
n-PENTANE	0.317
ISOPENTANE	0.408
n-HEXANE	0.417
n-HEPTANE	0.000

CNG = \$ Compressed Natural Gas  
LNG = \$ Liquefied Natural Gas  
LPG = \$\$ Liquefied Petroleum Gas  
Condensate = \$\$\$ Liquid Fuels



# Flare gas monetization— Rigorous thermodynamic validation

## Extract Solution

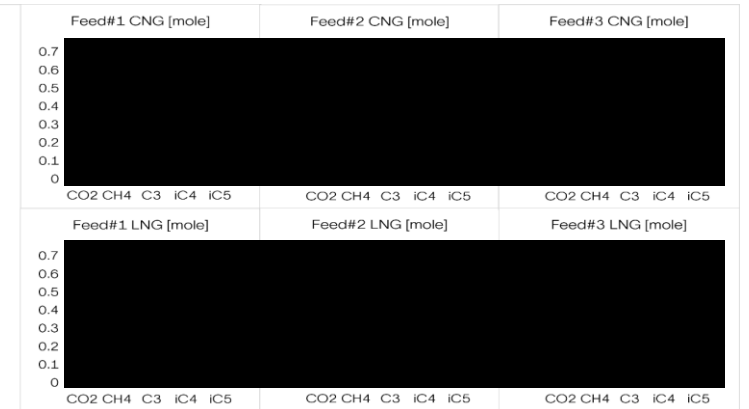
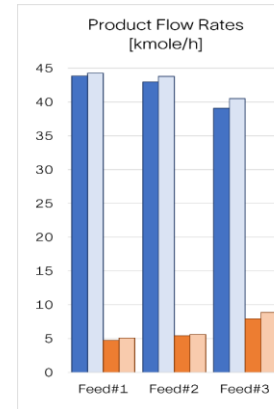


Internally developed process simulation software used to rigorously and accurately analyze each opportunity

## Fuels

- Compressed natural gas
- Liquefied natural gas
- Extracted natural gas liquids
- Liquid fuels
- Hydrogen

## Product Flow Match



CNG Composition Match

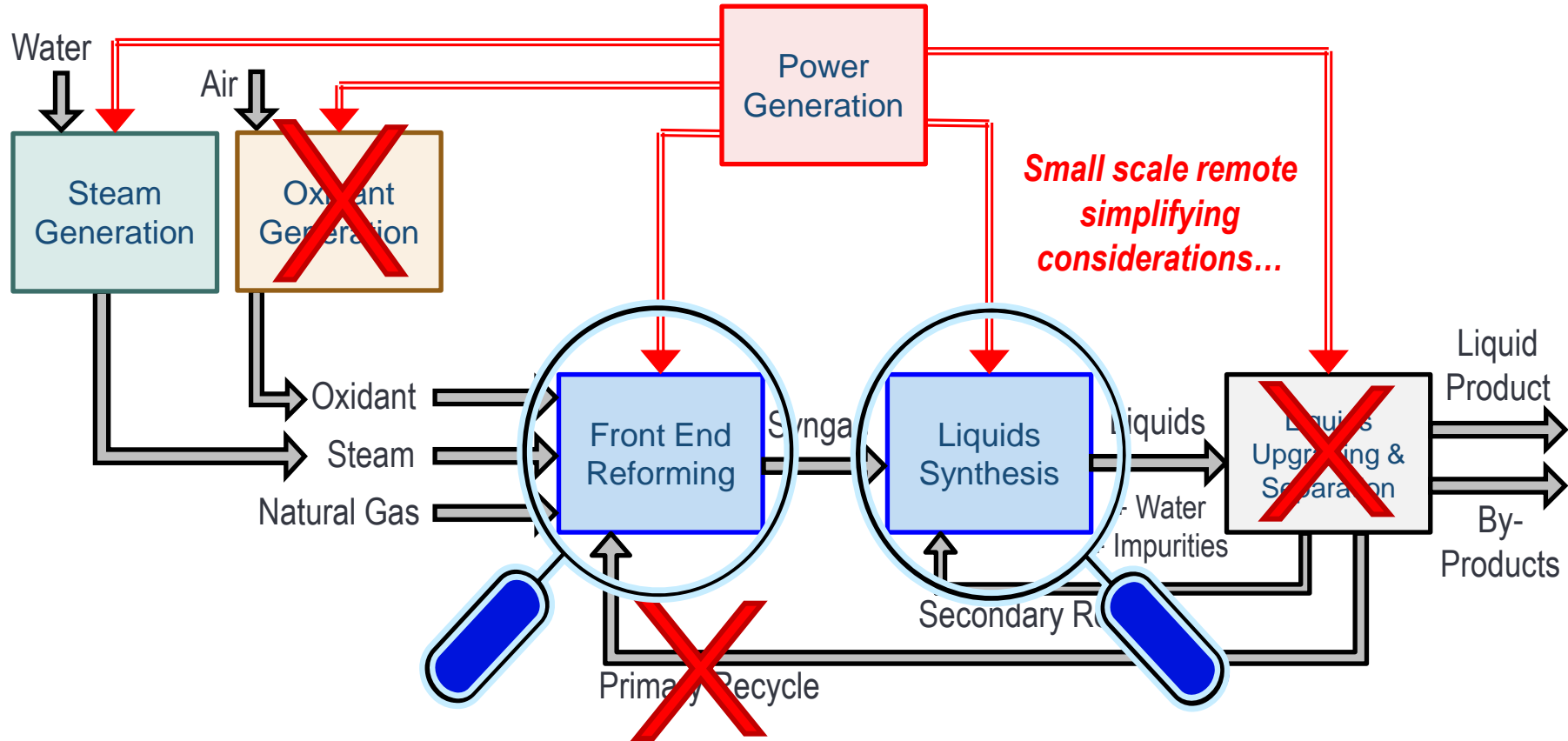
LNG Composition Match

■ Plant □ Simulation

■ Plant □ Simulation

# Gas to liquids—Synthetic liquids (methanol, synfuels) overview

Multiple considerations are required for the overall synthetic liquids production facilities

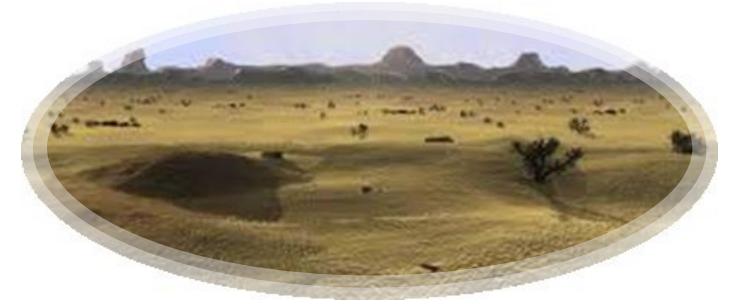


# Gas to liquids—Synthetic liquids front-end reforming



## How to pick the front-end reforming design?

Utilities available at stranded gas?  
Water, oxidant, power, etc.



*Either furnace  
or electrified* →

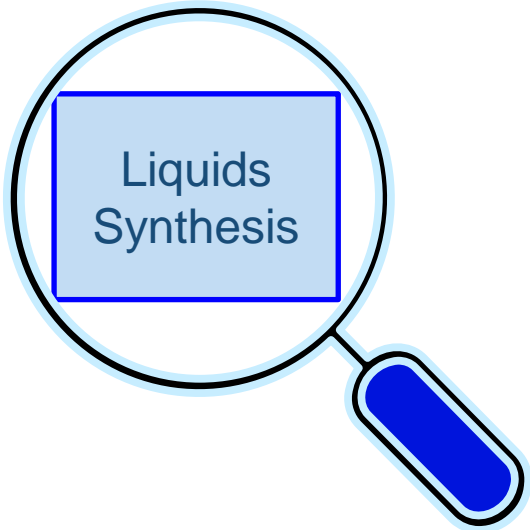
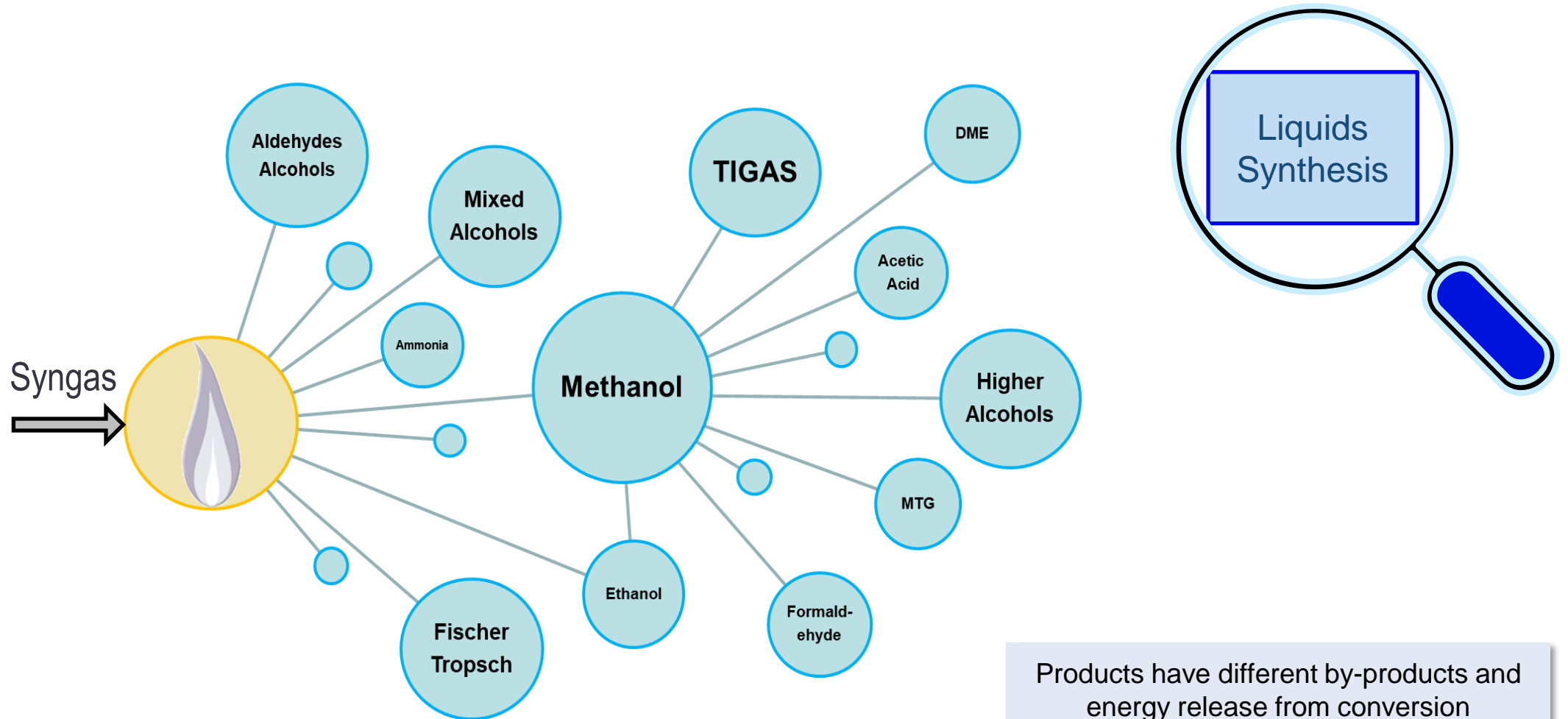
	Water	Oxidant	Syngas Impurity	Feed Pressure
<b>SMR</b>	High	None	Low	Medium
<b>ATR</b>	Small/None	High	High	High
<b>POx</b>	Small/None	Medium	Medium	Low
<b>Plasma</b>	None	None	Low	Medium

**SMR** = Steam methane reforming

**ATR** = Autothermal reforming

**POx** = Partial oxidization

# Gas to liquids—Synthetic liquids (methanol, synfuels) overview



Products have different by-products and energy release from conversion (and phase change)

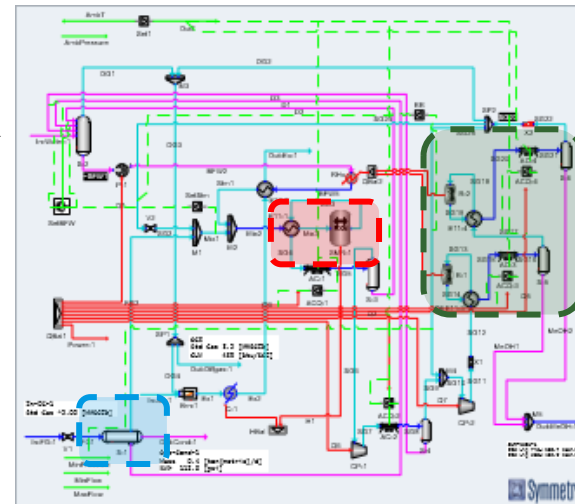
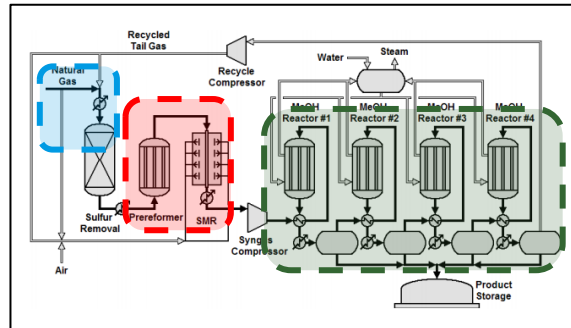
# Flare gas monetization— Rigorous thermodynamic validation

## Synfuel Solution

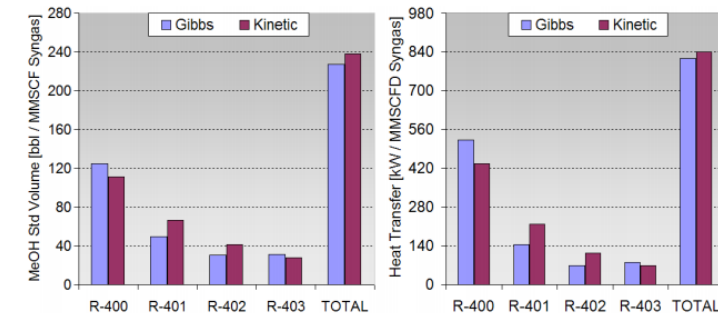


Internally developed process simulation software used to rigorously and accurately analyze each opportunity

- Fuels**
- Compressed natural gas
  - Liquefied natural gas
  - Extracted natural gas liquids
  - **Liquid fuels**
  - Hydrogen



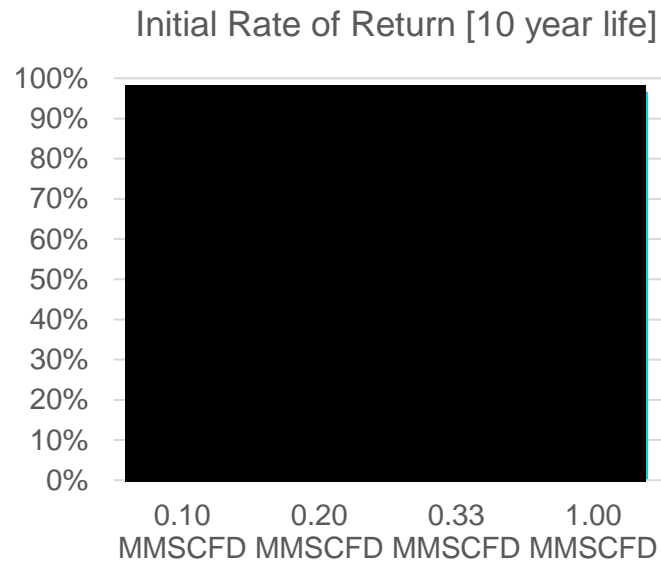
Product Flow Match



Hay et al, Chemical Product & Process Modeling(2011)

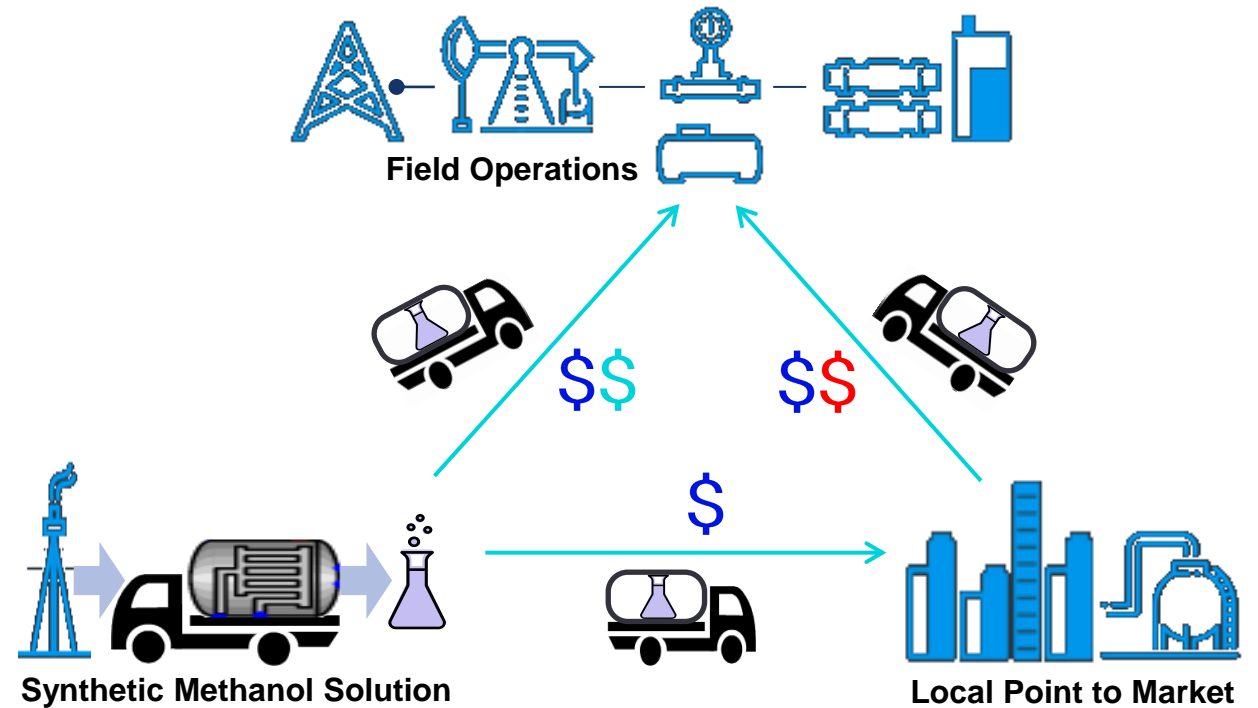


# Flare gas monetization— Specialty chemical with inventory and upgrading cost abatement

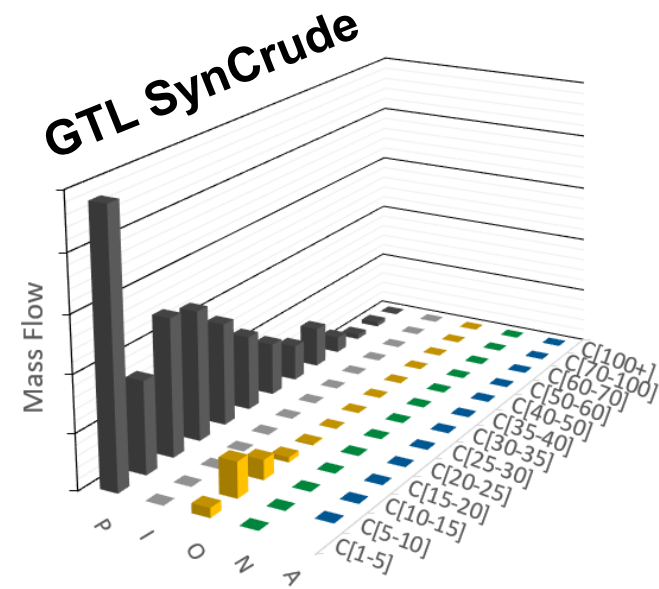
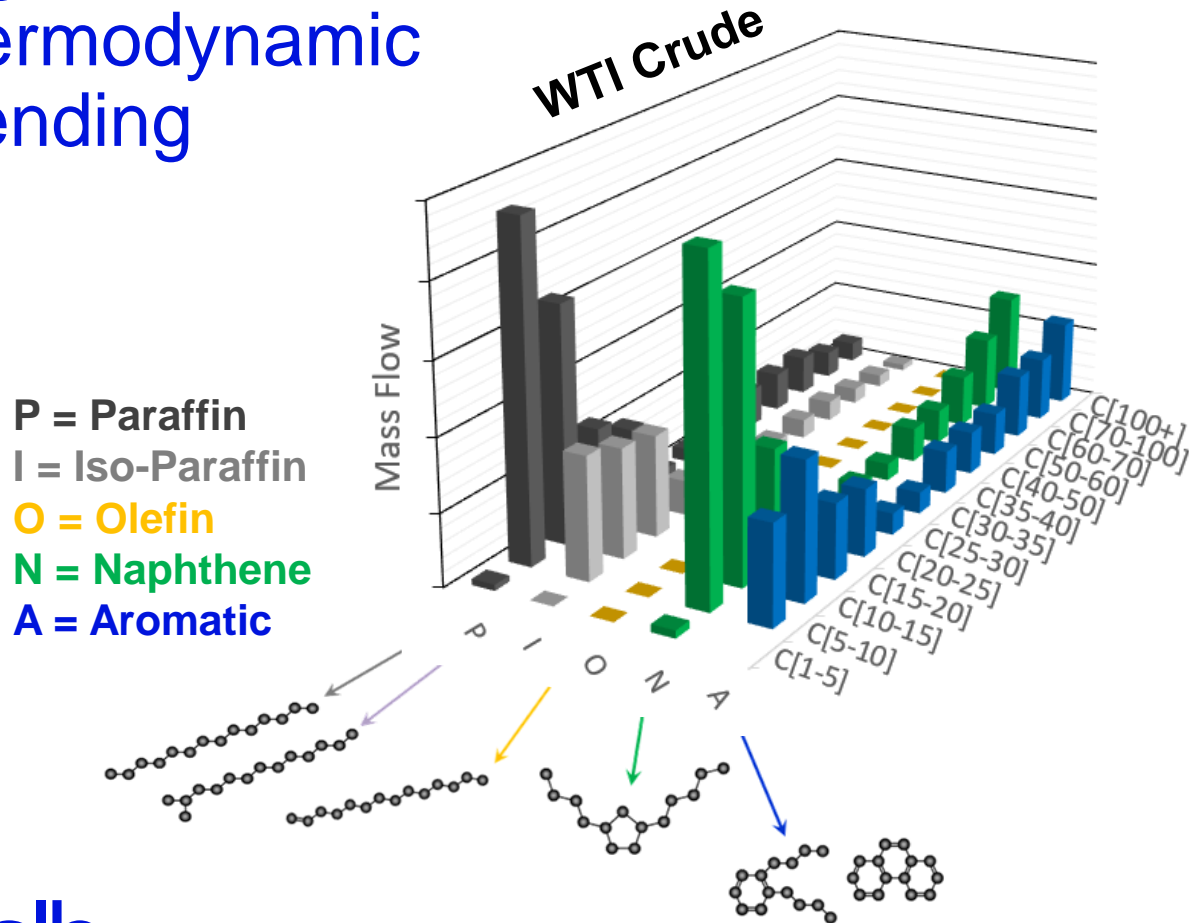


- Market Price @\$0.50/kg (~\$1.50/gal)
- Inventory Price @\$1.00/kg (~\$3.00/gal)

Market point price sometimes does not accurately represent the actual operational cost that could potentially be eliminated locally



# Flare gas monetization— Rigorous thermodynamic blending



## Pour Point Temperature

Cut Range, NBP [F]	WTI Crude	Syn Crude
Diesel [500- 650]	~ 15 F	█ F
Kerosene [350- 500]	~ -50 F	█ F

## Kinematic Viscosity @ 100F

Cut Range, NBP [F]	WTI Crude	Syn Crude
Diesel [500- 650]	~ 9.0 cSt	█ cSt
Kerosene [350- 500]	~ 3.0 cSt	█ cSt

More paraffins in fluid →

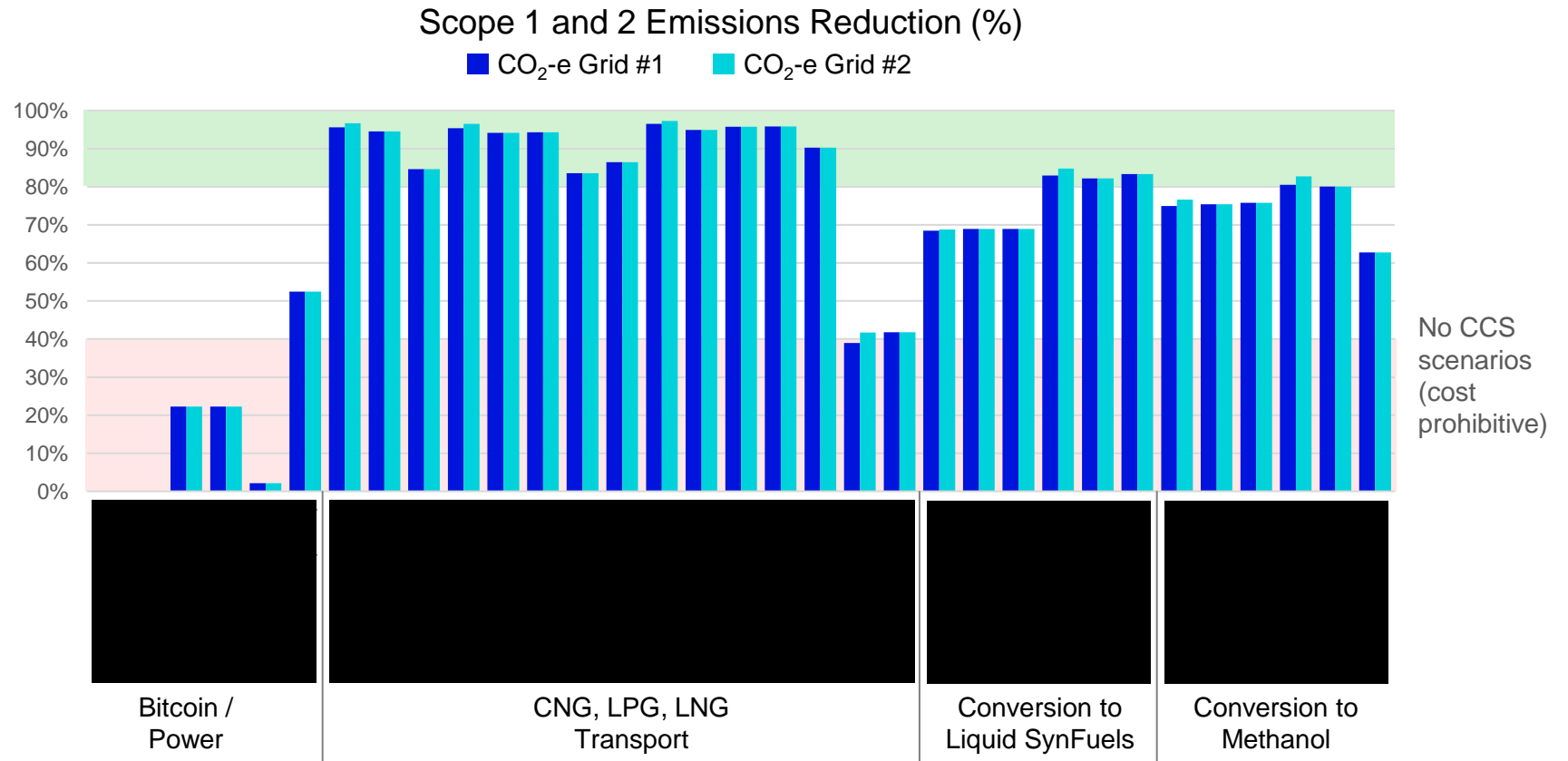


Simple index blending rules do not apply unless they account for molecular structure



# Flare gas monetization— Scenario scope 1 and 2 emissions reduction

CO<sub>2</sub> equivalent emission reduction based on 98% flare destruction efficiency  
(Methane GWP x25)

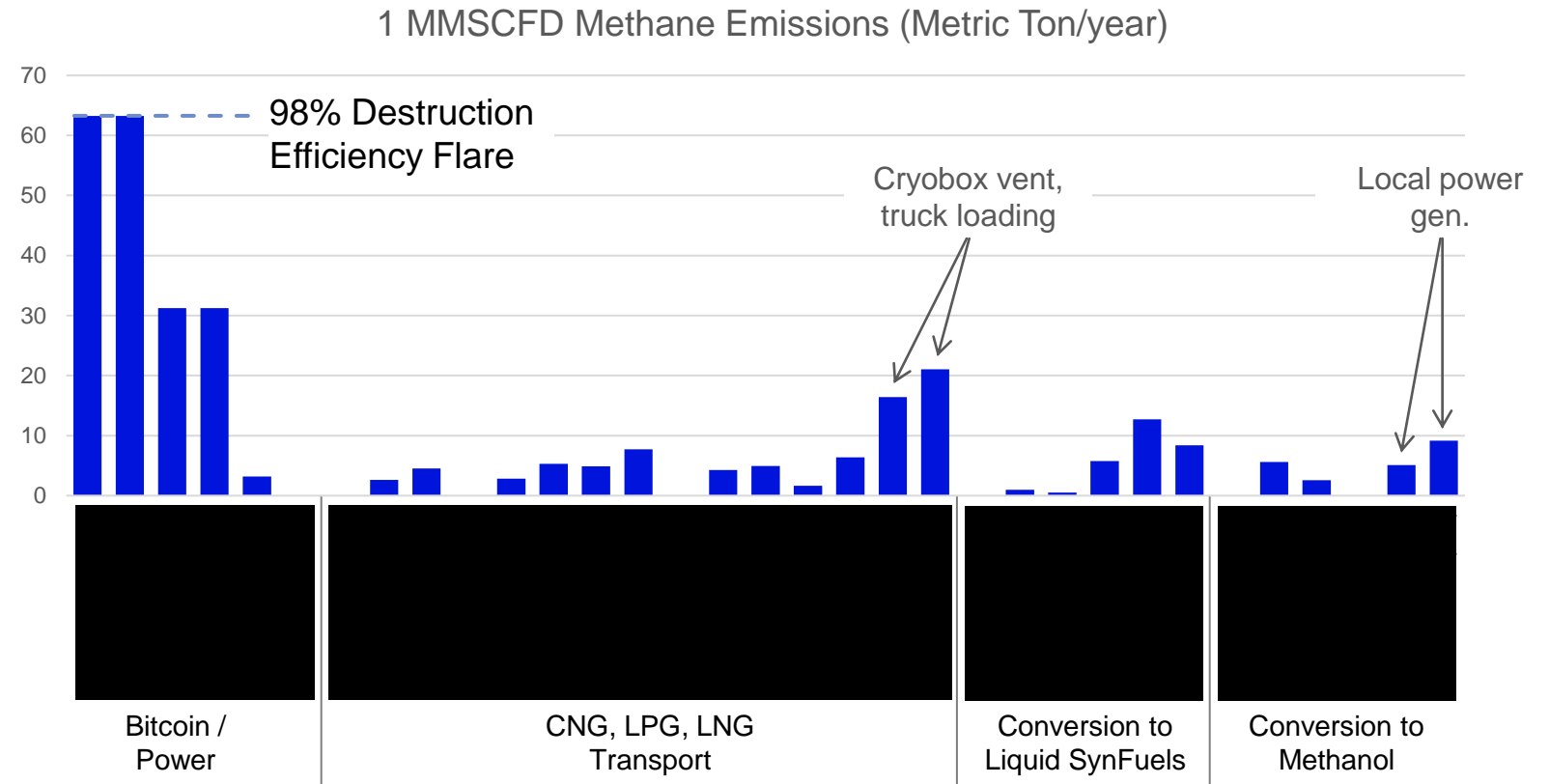


Solutions have varied resulting emission reductions



# Flare gas monetization— Scenario planned methane emissions

**Fugitive** methane can also be significant and minimized by monitoring programs, but some planned methane is process related due to venting, combustion, etc.



Solutions have varied reduction of resulting methane emissions



# Takeaways

- Plan-Measure-Act = Gas monetization with reduced emissions
- Complexities require developed methodologies and understanding to expediate the advisory for optimal returns
- Business strategy must keep up with emerging technology
- Local understanding needed to determine best solutions

Thank you, open Q&A discussions

